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ASYMMETRIC CELLULOSE ACETATE MEMBRANES USED IN SEPARATION APPLICATIONS

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ABSTRACT. This work focused on the use of cellulose acetate polymer for the preparation of porous asymmetric membranes using a phase inversion These membranes process. were characterised by scanning electron microscopy, a bubble-point method and sorption measurements. The preparation method used induced membrane anisotropy. The capacity of the membranes in the removal of electrolyte (NaCl) from aqueous solution was investigated. A good retention of 58.6% and a high flux rate of 8.9×10^{-4} m/s using NaCl solution of 200 mg/L concentration were obtained by cellulose acetate membranes prepared with water as non-solvent. The results showed that the membrane performance was affected by the membrane structure, which was determined by the conditions of membrane preparation.

Keywords: cellulose acetate polymer; porous membrane; asymmetric structure; salt rejection.

INTRODUCTION

Membrane processes are a good alternative to conventional water (Ladewig Al-Shaeli. 2017: and Peinemann Nunes, and 2010). Nanofiltration. reverse osmosis. microfiltration, ultrafiltration, etc. are membrane processes currently used to obtain drinking water and in the depollution of wastewater in order to protect the environment. One of the applications important verv of membrane filtration is water desalination, *i.e.*, the elimination of salts from seawater, but also the removal of toxic compounds existing in wastewater arising from various industries (Ciobanu et al., 2009; Ciobanu and Carja, 2010; Goh et al., 2016; Elimelech and Phillip, 2011).

Filter membranes, depending on their structure, can be symmetrical or

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asymmetrical, porous or non-porous. Also, depending on the materials from which they are made, the membranes can be polymeric, ceramic or polymerpolymer or polymer-ceramic composites.

A crucial moment in membrane technology was 1962, when Loeb and Sourirajan developed the phase inversion method obtaining for integrally skinned asymmetric membranes (Loeb and Sourirajan, 1962). This method involves the addition of a multicomponent solution (consisting of either a binary mixture of polymer and solvent or а combination of polymers, solvents, and non-solvents) in a coagulation bath (containing non-solvent а immiscible with the polymer). The counter diffusion between solvent and non-solvent leads to a phase instability in the solution, which results in the separation of the wet phase to form a membrane with an asymmetric structure (Ismail and Yean, 2003). The obtained membranes are formed by superimposed layers of different thicknesses and porosities: a top skin laver, a porous sub-laver (substructure) and a bottom skin (Ciobanu and Ciobanu, 2015; Kesting, 1985; Purkait et al., 2018).

In recent years, many studies have focused on the phase inversion process because it is one of the most versatile, economical and reproducible processes for forming polymeric asymmetric membranes (Baldino *et al.*, 2017). In recent years, many categories of polymers with specific properties have been used to obtain asymmetric membranes, which have led to various applications in the separation and purification processes. A very important aspect in the research carried out by the specialists in the membrane science is to obtain membranes with a higher selectivity and high flow (Gao et al., 2011; Huang et al., 2019; Khan et al., 2020). Cellulose acetate is a modified natural polymer with a wide range of properties applications (e.g., for films, and membranes or fibres) (Fischer et al., 2008). Cellulose acetate is used in the preparation of ultra- and nanofiltration membranes for gas or liquid separation applications due its to good hydrophilicity, high toughness, and low price (Idress et al., 2021). The hydrophilic nature of cellulose acetate is desirable in a membrane process: wetting the membrane reduces the concentration polarisation internal (and this reduces membrane fouling) and increases water flux.

This study investigated whether cellulose acetate sheets could be used as semipermeable membranes in water desalination. The membranes were produced by a very easy method based on the phase inversion process. Membrane characterisations, such as morphology and sodium chloride rejection are reported.

EXPERIMENTAL

Materials

Cellulose acetate with 39.8% acetyl content and average molecular weight Mn of ~30,000, acetone, formamide and NaCl were purchased from Sigma-Aldrich

(Germany). In the coagulation process, acetone acted as a solvent, while formamide or water acted as non-solvents. In order to evaluate the membrane performance in terms of percentage rejection and flux rate, NaCl solutions of different concentrations were prepared.

Membrane preparation

The membranes were prepared via the phase inversion method described elsewhere (Ciobanu and Bezdadea, 2004), starting from a 20 wt % cellulose acetate solution in acetone. Cellulose acetate and acetone were stirred in an Erlenmeyer flask until a homogeneous solution was formed (20-24 h). A fixed amount of nonsolvent (deionised water or formamide) was added slowly to the polymer solution and stirred for another 2-3 h. The solution was then cast at ambient temperature on a glass dish with a special stainless-steel cast knife. The thickness of the fabricated membrane was ~300-350 µm. As soon as possible, the thin layer of cast solution together with the glass plate was immersed in the coagulation bath of pure water. The membranes formed were left in the coagulation bath for 30-60 min and then transferred to deionised water until characterisation.

Membrane characterisation

The sample morphology was investigated by scanning electron microscopy (SEM) with a TESLA-BS-300 instrument. The pore sizes were estimated by the bubble-point method with a homemade laboratory instrument.

The permeation experiments were carried out in a dead-end flow cell using circular membranes with a 12.5 cm² effective area available for filtration. The flux rate and solute rejection were measured using NaCl solutions of different concentrations, at 25°C and at ~5 bar applied feed pressure. The conductivity of

the permeate was measured using a conductivity meter, model CONSORT C831. Parameters used to quantify the membrane performance were flux rate of the solutions J (m/s), and salt rejection R(%):

$$J = \frac{V}{t \cdot A} \quad (1)$$
$$R(\%) = \left[1 - \frac{C_p}{C_f}\right] \cdot 100 \quad (2)$$

where, V/t is volume permeation rate (m³/s), A is membrane area (m²), and C_p and C_f are the concentrations of the permeate and feed solutions, respectively.

RESULTS AND DISCUSSION

Generally, the morphology of a membrane (i.e., thickness or porosity) is influenced by the process parameters, which ultimately lead to certain separation performances of the membrane (Idris *et al.*, 2002; Wang *et al.*, 2006). Phase inversion is a good method for obtaining integrally skinned asymmetric membranes (Loeb and Sourrirajan, 1962; Strathmann *et al.*, 1975; Garcia *et al.*, 2020).

In our study, the obtained microporous membranes (i.e., CAM-F and CAM-W) have an open threedimensional structure in which the pores are of molecular size consisted of a three-dimensional polymeric structure with pore sizes of molecular dimensions, which offer specific permeability to a component in a process feed to the membrane. These membranes have a quite complex, open, colloidal-type structure with a small fraction of the membrane volume occupied by the polymer The cellulose substrate acetate

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membranes appeared to be a cohesive system consisting of open-cell foams (*i.e.*, vacuoles with branched walls) composed of a cellular network bound together by chainlike ribs extending in three dimensions. The SEM images of the cellulose acetate membranes were evidence of the asymmetry/ heterogeneity of these systems (*Fig. 1*).

All the membranes have an asymmetric structure consisting of several layered areas, namely: the active layer (an ultra-thin skin layer), the transition layer (an open-cell and substructure) finger-like and the bottom layer. As reported by Kestingm (Kesting, 1985), generally large fingermacrovoids and cavity-like like formed when the structures are coagulation process is rapid, whereas a slow coagulation rate results in a porous sponge-like structure. The coagulation took place rapidly (in ~15 min) when the polymer solution was brought into contact with cold water; this explained the finger-like structure of our membranes. In the active layer, the estimated pore size is much smaller than that of the supported layer and, therefore, due to these very small pores results the molecular sieve cellulose property of acetate membranes.

Accordingly, the molecular sieve property of cellulose acetate membranes appears to be determined by the pore size in the top layer of the membranes.

Some physical characteristics of the prepared cellulose acetate membranes are presented in *Table 1*.



Figure 1 - SEM images of cellulose acetate membranes in cross-section: a) CAM-F and b) CAM-W samples

Table 1 - Physical characteristics of the prepared	d
cellulose acetate membranes	

Characteristic	CAM-F*	CAM-W*
Thickness (µm)	240	375
Pore diameter in top surface (µm)	0.2-2.5	0.5-8.5
Void diameter in substructure (µm)	10-40	15-70

*The non-solvent was formamide (F) or water (W).

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In the first stage of the study, the pure water flux of the membranes was determined. At 25°C and 5-bar applied pressure, the pure water fluxes values for CAM-F and CAM-W samples were about 4.5×10^{-4} m/s and 5.3×10^{-4} m/s, respectively, showing that the pure water flux was increased for cellulose acetate membranes prepared with water as non-solvent (CAM-W sample).

In the second step, the capacity of the membranes for electrolyte (NaCl) removal from aqueous solution was investigated. The results, in terms of flux rate (J) and percentage rejection (R%) are presented in **Table 2**, showing that the flux and percentage rejection were increased for cellulose acetate membranes obtained by using water as non-solvent (CAM-W sample).

 Table 2 - Performance of the prepared cellulose acetate membranes

	Membrane				
Characteristic	CAM-F		CAM-W		
Characteristic	Concentration of NaCl solution (mg/L)				
	10	200	10	200	
J (m/s) × 10 ⁻⁴	7.2	7.4	8.3	8.9	
R% (%)	49.3	51.2	55.1	58.6	

According to the obtained results it can be observed that the performances of the analysed membranes are influenced by the membrane structure that depends on the conditions of membrane preparation, the composition of the casting solution being very important. During the phase inversion processes, due to some phenomena of microphase separation in the of evaporation and/or quenching of the polymeric solution, the formation of asymmetric cellulose the acetate membrane takes place.

Considering the experimental results, it can be concluded that these asymmetric cellulose acetate membranes can be used in various separation processes, especially for the removal of electrolytes from wastewater.

CONCLUSION

Asymmetric porous cellulose acetate membranes were prepared via a phase inversion method starting from a 20 wt % cellulose acetate solution in acetone to which a fixed amount of non-solvent (deionised water or formamide) was added. The cellulose acetate membranes consist of several layered areas, namely: the active layer (an ultra-thin skin layer), the transition laver (an open-cell and finger-like substructure) and the bottom layer The results showed that the membrane performance was affected by the membrane which structure. was determined by the conditions of membrane preparation, *i.e.*, the nature of the non-solvent in the casting solution. In this study, cellulose acetate membranes prepared from a ternary system consisting of cellulose

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acetate, acetone and water using a phase inversion process were appropriate for a water desalination process. They showed a good pure water flux and a moderate percentage of rejection using a NaCl solution of 200 mg/L concentration.

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